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Numerical Problem

~~CHENG324 Lecture20~~

~~Chapter 5 Solving~~

~~Solving Problems~~

~~5.2,5.3,5.4,5.5~~ Process

Dynamics and

Control -Objective

Type Questions |

Chemical

Engineering | Umang

Goswami ~~CHENG324~~

~~Lecture21 Chapter 5~~

~~Solving Problems 5 6,~~

~~5 8, 5 9, 5 10~~ Process

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Dynamics /u0026

Control for GATE

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Solution of Process

Dynamic and Control

Worked problem

Seborg 17.8 (sampled
temperature signal)

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~~Chapter 5 Solving~~

~~Problems 5-12 to 5-20~~

Detailed Video

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Solution of PDC, CRE
and PDEco Questions

~~Process Control: 1-3~~

~~Process Dynamic~~

~~(Gain, Time Constant,~~

~~Dead Time)~~ Linear

Regression - Fun and

Easy Machine

Learning Process

Dynamics and

Control linearisation

of nonlinear system

behaviour of first

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MIXING PROCESS

Problem 5.3 Process
systems analysis and
control by Leizel

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rectangular pulse

forcing function

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Dynamics with

Graphical Fit

Blending Process:

Linearization

Example GATE 2017

Detailed Solutions-

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Problems on

Obtaining Transfer

Functions Linear

regression and curve

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Decoupling Control

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solution: There are three important process variables in a process control system. Feedback control system measures the controlled variable and compares the measured value with the desired value and then adjusts the manipulated

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variables for the
control of the system
accordingly.

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Variables : w_1 , w_2 ,
 T_1 , T_2 , T_3 . $NE = 1$
 $NV = 5$. Thus, $NF = 5$

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$\tau_1 = 4$. Because w_1 , w_2 , T_1 and T_2 are determined by upstream units, we assume they are known functions of time: $w_1 = w_1(t)$, $w_2 = w_2(t)$

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Control

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Solution:(a) For outer
tank $WC(T_i - T_o) +$
 $hA (T_1 - T_2) - WC(T_2$
 $- T_o) = C$

$V_2 \frac{dT_2}{dt}$ ----- (1) At
steady state $WC(T_{1s} -$
 $T_o) + hA (T_{1s} - T_{2s}) -$

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Process

$$WC(T_2s - T_o) = 0 \text{ -----}$$

$$(2)(1) - (2)$$

$$\text{gives } WC T_i' + hA$$

$$(T_1' - T_2') -$$

$$WC T_2' = C$$

$V_2 dt dT_2$ Substituting

numerical values 10

$$T_i' + 10 (T_1' -$$

$$T_2') - 10 T_2' =$$

$$50 dt dT_2$$
 Taking

$$\text{L.T. } T_i(s) + T_1(s) -$$

$$2T_2(s) = 5 s T_2(s)$$
 Now

$$T_i(s) = 0, \text{ since there}$$

is no change in temp

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of feed stream to
outer tank.

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